

GAS FORM-C
based on the
OCIMF / SIGTTO
SHIP INFORMATION QUESTIONNAIRE
for
GAS CARRIERS
2nd Edition 1998

Specifications of the vessel and the gas installations are believed to be correct, but not guaranteed.

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**SECTION A
GENERAL INFORMATION**

A1 PRINCIPAL SHIP PARTICULARS

1,1	Date questionnaire completed	13-Jun-16
1,2	Name of vessel	JS GREENSTAR
1,3	LR/IMO number	9540003
1,4	Last previous name	N/A
1.4.1	Date of name change	N/A
1,5	Second last previous name	N/A
1.5.1	Date of name change	N/A
1,6	Third last previous name	N/A
1.6.1	Date of name change	N/A
1,7	Fourth last previous name	N/A
1.7.1	Date of name change	N/A
1,8	Flag	Malta
1,9	Port of Registry	Valletta
1.10	Official number	9540003
1,11	Call sign	9HA3302
1,12	INMARSAT A or B number	N/A
1,13	Vessel's telephone number	870 773 240 880
1.13.1	Vessel's mobile number	+65 9721 6137
1,14	Vessel's fax number	870 783 222 384
1,15	Vessel's telex number	N/A
1,16	Vessel's E-mail address	js.greenstar@thomships.net
1,17	INMARSAT C number	422 939 910 422 939 911
1,18	Vessel's MMSI number	229 399 000
1,19	Type of vessel	LPG/LEG Carrier

OWNERSHIP AND OPERATION

1.20	Registered Owner	GREENSHIP GAS SAS
	Full address	2 RUE BENOIT MALON 92150 SURESNES FRANCE
	Office telephone number	+356 21 241232
	Office telex number	N/A
	Office fax number	+356 25 990642
	Office Email address	pbe@greenshipgas.com
	Contact person	Mihir Navalkar
	Contact person after hours telephone number	+33158470346
1.21	Name of technical operator (If different from above)	Evergas Ship Management Pte Ltd
	Full Address	16 Raffles Quay, #43-01 Hong Leong Building Singapore 048581
	Office telephone number	+65 6220 7291
	Office telex number	N/A
	Office fax number	+65 6225 1527
	Office Email address	rkr@evergas.net
	Contact person (Designated Person Ashore)	Rajneesh Rana
	Contact person after hours telephone number	+65 9113 3759
	Emergency callout number	+65 8188 8482
	Emergency callout pager number	N/A
	Contact details for person responsible for oil spill response	Rajneesh Rana
	Number of years controlled by technical operator	0

1.22	Total number of ships operated by this Operator	19
1.23	Number of years ship owned	1
1.23.1	Name of commercial operator (If different from above)	Evergas Management A/S
	Full Address	Kalvebod Brygge 39-41 1560 Copenhagen
	Office telephone number	+ 45 3997 0372
	Office telex number	N/A
	Office fax number	N/A
	Office Email address	operations@evergas.net
	Contact person	Nete Egebjerg
	Contact person after hours telephone number	+45 3038 1156
	Emergency callout number	+4539970101
	Emergency callout pager number	N/A
	Number of years controlled by commercial operator	3

BUILDER

1.24	Builder	Nantong Sinopacific Offshore & Engineering
1.25	Name of yard vessel built at	SOE
1.26	Hull number (Class ID No.)	S1007
1.27	Date keel laid	23-Mar-12
1.28	Date launched	20-Aug-12
1.29	Date delivered	2-May-13
1.30	Date of completion of major hull changes, - if any.	N/A
1.31	If changes were made, what changes were made and at which yard were they carried out	N/A

CLASSIFICATION

1.32	Classification society	BV
1.33	Class Notation	IHULLMACH Liquefied gas carrier; FLS tanker, Unrestricted navigation, AUT- UMS, MON-SHAFT, BWE, BWT CLEANSHIP, INWATERSURVEY, IC
1.34	If Classification society changed, name of previous society	GL
1.35	If Classification society changed, date of change	27.04.2016
1.36	Was ship built in accordance with the following regulations:	

	IMO	Yes
	US COAST GUARD	Yes
	IACS Class	Yes
	Other: <u>ILO Convention Nr. 92 &133; MLC, 2006</u>	Yes
1.37	IMO certification	
	Certificate of fitness - IGC	Yes
	Certificate - A328	N/A
	Certificate - A329	N/A
	Letter of Compliance	nil
	Issued by	
1.38	Unattended Machinery Space Certificate	N/A (included in Class)
1.39	Net Registered Tonnage	3,846
1.40	Gross Registered Tonnage	12.819
1.41	Suez Net Tonnage - Canal Tonnage	11.539,02
	Suez Gross Tonnage	14.148,97
1.42	Panama Net Tonnage - Canal Tonnage	10.772
	Panama Gross Tonnage	N/A

A2 HULL DIMENSIONS

2.1	Length overall (LOA)	142,54	Metres
2.2	Length between perpendiculars (LBP)	134,62	Metres
2.3	Distance bow to bridge	112,00	Metres
2.4	Distance bridge front - mid point manifold	38,00	Metres
2.5	Distance bow to mid-point manifold	74,00	Metres
2.6	Extreme breadth	21,60	Metres
2.7	Extreme depth	12,10	Metres
2.8	Summer draught (design / Scantling)	9,51	Metres
2.9	Corresponding Summer deadweight	15210,7	Tonnes
2.10	Light displacement	6960,0	Tonnes
2.11	Loaded displacement (Summer deadweight)	22170,7	Tonnes
2.12	Cargo tanks cubic capacity - 100%	12057,06	Cubic metres
2.12.1	Deck tank(s) cubic capacity - 100%	N/A	Cubic metres
2.12.2	Cargo tanks cubic capacity - 98%	11815,92	Cubic metres
2.12.3	Deck tank(s) cubic capacity - 98%	N/A	Cubic metres
2.13	Distance from keel to highest point	42,00	Metres
2.14	Air draught (normal ballast condition)	36,10	Metres

A3 IMMERSION

3.1	TPC - in normal ballast condition	23,8	27,6
	TPC - in loaded condition (summer deadweight)	5,4	9,5

Tonnes / cm @ metres draught

A4 LOADED PARTICULARS

	N-Butane	C-Propane	
4.1	Cargo grade		
4.2	Density	0,6018	0,583 Tonnes/m3
4.3	Cargo loadable	7.111	6.889 Tonnes
4.4	Bunkers - FO	1230,5	1230,5 Tonnes
4.5	Bunkers - DO	307,2	307,2 Tonnes
4.6	Fresh water	277,9	277,9 Tonnes
4.7	Stores & spares	10	10 Tonnes
4.8	Lub oil	56,9	56,9 Tonnes
4.9	Ballast	1851	2095 Tonnes
4.10	Deadweight	10.845	10867 Tonnes
4.11	Draught - forward	7,19	7,38 Metres
	Draught - aft	8,53	8,34 Metres
	Draught - mean	7,86	7,86 Metres

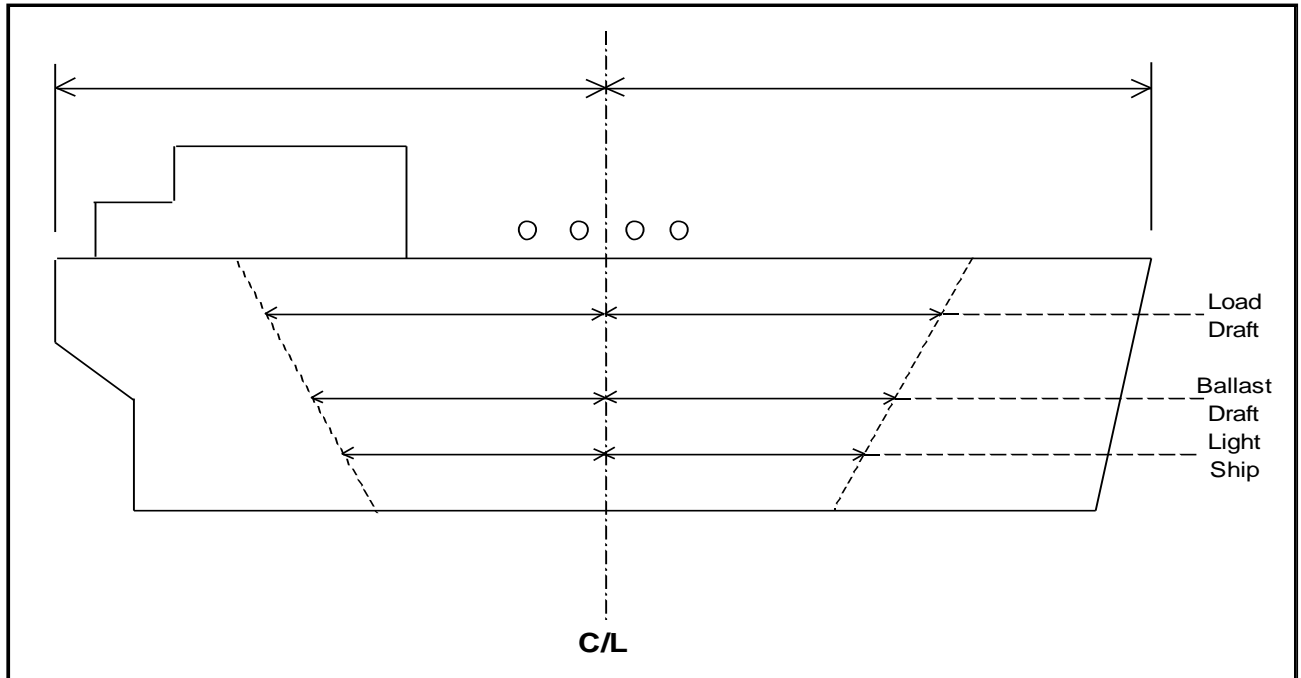
	Butadiene	Propylene	
	Cargo grade		
	Density	0,6503	0,6091 Tonnes/m3
	Cargo loadable	7684	7197 Tonnes
	Bunkers - FO	1230,5	1230,5 Tonnes
	Bunkers - DO	307,2	307,2 Tonnes
	Fresh water	277,9	277,9 Tonnes
	Stores & spares	10	10 Tonnes
	Lub oil	56,9	56,9 Tonnes
	Ballast	1851	2095 Tonnes
	Deadweight	11418	11175 Tonnes
	Draught - forward	7,55	7,6 Metres
	Draught - aft	8,62	8,38 Metres
	Draught - mean	8,08	7,98 Metres

	Ethylene	Ammonia	
Cargo grade			
Density	0,568	0,6735	Tonnes/m3
Cargo loadable	6711	7958	Tonnes
Bunkers - FO / LNG	1230,5	1230,50	Tonnes
Bunkers - DO	307,2	307,2	Tonnes
Fresh water	277,9	277,9	Tonnes
Stores & spares	10	10	Tonnes
Lub oil	56,9	56,9	Tonnes
Ballast	2218	2278	Tonnes
Deadweight	10812	12119	Tonnes
Draught - forward	7,72	7,67	Metres
Draught - aft	8,04	8,29	Metres
Draught - mean	7,87	8,85	Metres

	VCM	Propylene Oxide	
Cargo grade			
Density	0,969	0,833	Tonnes/m3
Cargo loadable	11450	7497	Tonnes
Bunkers - FO	1230,5	1230,5	Tonnes
Bunkers - DO	307,2	307,2	Tonnes
Fresh water	277,9	277,9	Tonnes
Stores & spares	10	10	Tonnes
Lub oil	56,9	56,9	Tonnes
Ballast	992,6	1235,9	Tonnes
Deadweight	14325	10615	Tonnes
Draught - forward	9,08	7,01	Metres
Draught - aft	9,25	8,42	Metres
Draught - mean	9,17	7,72	Metres

	Ballast		
Cargo grade			
Density			Tonnes/m3
Cargo loadable			Tonnes
Bunkers - FO	372,8		Tonnes
Bunkers - DO	36,4		Tonnes
Fresh water	115,3		Tonnes
Stores & spares	5,5		Tonnes
Lub oil	56,8		Tonnes
Ballast	3863		Tonnes
Deadweight	4449,8		Tonnes
Draught - forward	4,99		Metres
Draught - aft	5,78		Metres
Draught - mean	5,39		Metres

A5 PARALLEL MID-BODY DIMENSIONS



5.1	Light ship	47	Metres
5.2	Forward to mid-point manifold - light ship	22	Metres
5.3	Aft to mid-point manifold - light ship	25	Metres
5.4	Normal ballast	52,5	Metres
5.5	Forward to mid-point manifold - normal ballast	24	Metres
5.6	Aft to mid-point manifold - normal ballast	28,5	Metres
5.7	Loaded SDWT	72	Metres
5.8	Forward to mid-point manifold - loaded SDWT	30	Metres
5.9	Aft to mid-point manifold - loaded SDWT	42	Metres

A6 BUNKER CAPACITIES

	Grade	Capacity @ 98%
Main engine	HFO	1353,1
Auxiliary engine(s)	MDO	208,7
Other: LSDO	LSDO	197,2

A7 FUEL CONSUMPTION DETAILS

	Grade		
7.1	At sea - normal service speed	HFO	Tonnes/day
		Diesel oil	Tonnes/day
		Gas oil	Tonnes/day
7.2	At sea - normal service speed - while conditioning cargo full cooling	HFO	Tonnes/day
		Diesel oil	Tonnes/day
		Gas oil	Tonnes/day
7.3	In port - loading	HFO	Tonnes/day
		Diesel oil	Tonnes/day
		Gas oil	Tonnes/day
7.4	In port - discharging	HFO	Tonnes/day
		Diesel oil	Tonnes/day
		Gas oil	Tonnes/day
7.5	In port - idle	HFO	Tonnes/day
		Diesel oil	Tonnes/day
		Gas oil	Tonnes/day

Remark: the fuel consumption details are based on the little operational experience that is available at this time.

A7 SPEED/CONSUMPTION

Copies of the vessel's Speed and Consumption Graph for both Laden and Ballast conditions are enclosed?

NO

A8 MAIN ENGINE PARTICULARS

8.1	Main engine make and type	MAN B&W 6S42MC7.1-TII	
		Two stroke	
8.2	Number of units	1	
8.3	Maximum continuous rating (MRC) per engine	6.100	133 r/min
8.4	Total available power - Kwe		6.100 kW
8.5	Normal service power - Kwe at 90% SMCR		5.490 kW

A9 AUXILIARY PLANTS

9.1	Make and type of auxiliary generators / engines	MAN 7L23/30H	
		Four stroke	
9.2	Number of units	3	
9.3	Maximum generator output per unit	RPM	Kilowatts
	Unit no. 1	900	1050 kW
	Unit no. 2	900	1050 kW
	Unit no. 3	900	1050 kW
9.4	Shaft generator		N/A
9.5	Total available power		N/A
9.6	Emergency generator	1800	120 kW
9.7	Emergency fire pump - type	Motor driven vertical centrifugal	
	Delivery pressure		8 bar
	Motive power		Electrical
	If electrical, - indicate power required		19,4 kW
9.8	Steering gear - type	Rotatory type - Rolls Royce SR-723-FCP	
	Indicate power required to steer the vessel with one pump unit		19 kW

A10 POWER/SPEED INFORMATION

10.1	Trial data	BHP	6008	kW
		MRC	5407	kW
		Speed	16,36	KN
		Draught	5,5	M
10.2	Normal service speed (LOADED / BALLAST)	BHP	6100	kW
		MRC	5490	kW
		Speed		KN
		Draught	9,5	M

A11 THRUSTERS

11.1	Make and type	Suzhou STT 002 FP	
11.2	Bow thruster	(output)	750 kW
11.3	Stern thruster	(output)	N/A

A12 FRESH WATER

12.1	Capacity of distilled tanks		59,1	Cubic metres
12.2	Capacity of domestic tanks		218,8	Cubic metres
12.3	Daily consumption	Distilled	1	Tonnes
		Domestic	7	Tonnes
12.4	Daily evaporator capacity		15	Tonnes

A13 BALLAST CAPACITIES AND PUMPS

Tank	Capacity (m3)	Number
13.1 Fore peak	261,1	FPT
13.2 Wing and or side tanks	3664,2	2-9 P+S/S
13.3 Double bottom tanks	608,5	1-4 C
13.4 Aft peak	259,6	APT
13.5 Deep tank	177,1	1
13.6 Total	4970,5	23

13.7 Ballast pump make and type	Centrifugal, Allweiler, MA 80-315/01	
13.8 Number of pumps	2	
13.9 Total capacity	500 m3/h	
13.10 Location	ENGINE ROOM	
13.11 Control location	Local, ECR, CCR	
13.13 Ballast Water Treatment Plant	1 unit	700 m3/h

A14 MOORING EQUIPMENT

14.1 ROPES

Indicate on the diagram below the position of:

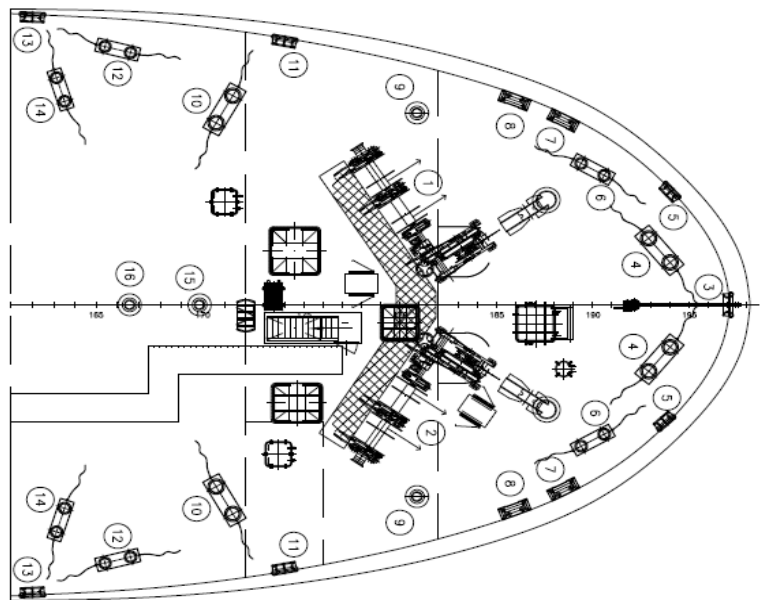
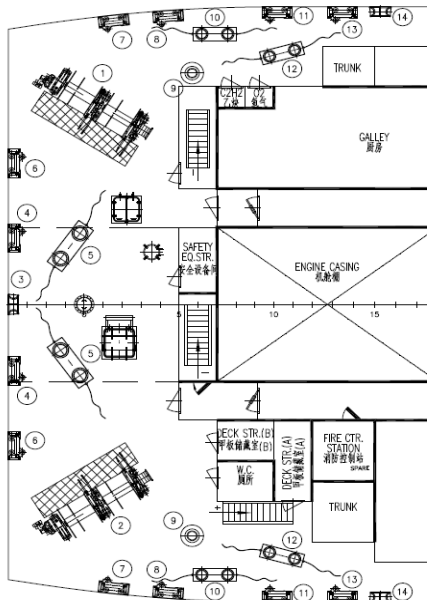
Winch Mounted Ropes (R)

Open Fairleads (O)

Closed Fairleads (C)

Alternatively enclosed copy of vessel's Mooring arrangements in A4 format.

NO



MOORING ROPES (ON DRUMS)

Mooring Ropes (On Drums) Forecastle - Number

Diameter

Material

Length

Breaking Strength

Mooring Ropes (On Drums) Forward Main Deck - Number

Diameter

Material

Length

Breaking Strength

	4	
	56 mm	MM
	Polyester & Polypropylene Mix	
	190 m	M
	37,8	MT
	0	
	N/A	
	N/A	
	N/A	
	N/A	

Mooring Ropes (On Drums) Aft Main Deck - Number	0	
Diameter	N/A	
Material	N/A	
Length	N/A	
Breaking Strength	N/A	
Mooring Ropes (On Drums) Poop - Number	4	
Diameter	56	MM
Material	Polyester & Polypropylene Mix	
Length	190	M
Breaking Strength	37,8	MT

OTHER MOORING LINES

Mooring Ropes not on Drums - Number	12	
Diameter	56 / 44	MM
Material	Polyester & Polypropylene Mix	
Length	190 / 220	M
Breaking Strength	37.8 / 44.0 / 47.7	MT
Emergency Towing Wires / Fire Wires - Number	2	
Diameter	24	MM
Material	Steel Wire, Galvanized	
Length	25	M
Breaking Strength	32	MT

14.2

MOORING WINCHES

Forecastle - Number	2	
Single Drum or Double Drums	Double drum	
Split Drums Y/N	Yes	
Motive Power	Electro/Hydraulic	
Heaving Power	10 mt	
Brake Capacity	31.8 mt	
Hauling Speed	15 m/min	
Forward Main Deck - Number	0	
Single Drum or Double Drums	N/A	
Split Drums Y/N	N/A	
Motive Power	N/A	
Heaving Power	N/A	
Brake Capacity	N/A	
Hauling Speed	N/A	
Aft Main Deck - Number	0	
Single Drum or Double Drums	N/A	
Split Drums Y/N	N/A	
Motive Power	N/A	
Heaving Power	N/A	
Brake Capacity	N/A	
Hauling Speed	N/A	
Poop - Number	2	
Single Drum or Double Drums	Double drum	
Split Drums Y/N	Yes	
Motive Power	Electro/Hydraulic	
Heaving Power	10	mt
Brake Capacity	22.2 mt	
Hauling Speed	15 m/min	

14.3

ANCHORS AND WINDLASS

Windlass motive power(e.g. steam, hydraulic)	Electro/Hydraulic	
Hauling power	149	kN
Brake holding power	1094	kN
Anchor type	Stockless	
Weight	3940	kg

	Is spare anchor carried		No	
	Cable diameter		56	mm
	Number of shackles port cable		10	
	Number of shackles starboard cable		11	
14.4	TOWING ARRANGEMENTS			
	Is the vessel fitted with a Towing Bracket Aft?		No	
		If Yes, state SWL	N/A	
	Is Towing chain provided		No	
	Dimensions of Towing wire	Diameter	N/A	
		Length	N/A	
14.5	WINDAGE			
	Windage on ballast draught	Front	510	M2
		Lateral	1998,2	M2
	Windage on loaded draught	Front	419,3	M2
		Lateral	1424	M2
A15	NAVIGATIONAL EQUIPMENT			
15.1	Magnetic compass		Yes	
15.2	Off Course Alarm - Magnetic compass		Yes	
15.3	Gyro compass		Yes	
		Number of Units	1	
15.4	Off Course Alarm - Gyro compass		Yes	
15.5	Gyro (Bridge) Repeaters		Yes	
		Number of Units	4	
15.6	Radar 3cm		Yes	
15.7	Radar 10cm		Yes	
15.8	Are radars gyro stabilised?		Yes	
15.9	Radar plotting equipment		Yes	
15.10	ARPA		Yes	
15.11	ECDIS		Yes	
15.12	Depth sounder with recorder		No	
15.13	Depth sounder without recorder		Yes	
15.14	Speed/distance indicator		Yes	
15.15	Doppler log		Yes	
15.16	Docking approach Doppler		No	
15.17	Rudder angle indicator		Yes	
15.18	Rudder angle indicator on Each Bridge Wing		Yes	
15.19	RPM indicator		Yes	
15.20	RPM indicator on Each Bridge Wing		No	
15.21	Controllable pitch propeller indicator		N/A	
15.22	Thruster(s) indicator		Yes	
15.23	Rate of turn indicator		No	
15.24	Radio direction finder		No	
15.25	Navtex receiver		Yes	
15.26	GPS		Yes	
15.26.1	DGPS		Yes	
15.27	Transit SATNAV		No	
15.28	Decca navigator		No	
15.29	Omega		No	
15.30	Loran C		No	
15.31	Weather fax		Yes	
15.32	Sextant(s)		Yes	
15.33	Signal lamp ALDIS		Yes	
15.34	Anemometer		Yes	
15.35	Engine order recorder		Yes	
15.35.1	VDR (Voyage Data Recorder)		Yes	
15.36	Course recorder		Yes	
15.37	Are steering motor controls and engine controls fitted on bridge wings?		Yes	

15.38	Is bridge equipped with a 'Dead-Man' alarm?		Yes
15.39	What chart outfit coverage is provided	World-wide	Yes
		Limited	No
	If limited, - please indicate area(s) covered		
15.40	Formal chart correction system in use		Yes
15.41	Electronic Chart system in use		Yes

A16 COMMUNICATIONS AND ELECTRONICS

16.2	What GMDSS areas is the vessel classed for? A1 A2 A3 A4		A1, A2 & A3
16.3	Transponder (SART)		Yes
16.4	EPIRB		Yes
16.5	How many VHF radios are fitted on the bridge?		2 + 2 bridge wing sockets
16.6	Is vessel fitted with VHF in the cargo control room (CCR)?		Yes
16.7	Is the CCR connected to the vessel's internal communication system?		Yes
16.8	How many intrinsically safe walkie talkies are provided for cargo handling?		10
16.9	Is vessel fitted with an INMARSAT satellite communications system?		Yes
16.10	Does vessel carry at least three survival craft two-way radio telephones?		Yes
16.11	Inmarsat satellite system		Yes
	Specify system type A, B or C		C
16.12	2182kHz bridge auto alarm		Yes
16.13	Radio telephone distress frequency watch receiver		Yes
16.14	Emergency lifeboat transceiver		Yes
16.15	Can vessel transmit the helicopter homing signal on 410 kHz?		No
16.16	Full set of Radio List publications		Yes

SECTION B CARGO SYSTEMS

B1 CARGO - GENERAL INFORMATION

1.1 List products which the ship is Certified to carry

Cargo	Temp at atm. Press (Celcius)	Density at atm. Press (kg/m3)
Ethylene	-104	568
Ethane	-89	545
Propylene	-48	609
Propane (pure)	-42	581
C-Propane (2,5 mol% ethane in Liq. Phase)	-45	583
Mix of propane and butane	-	-
Anhydrous Ammonia	-33	673
VCM	-14	969
Iso-Butane	-12	594
Butylenes (data for Iso)	-7	625
Butadiene	-5	650
N-Butane	0	602
DME	-25	734
Other Cargoes		
Acetaldehyde	20	778
Dimethyl Amine	7	666
Ethyl Chloride	13	903
Diethyl Ether	35	700
Isoprene (Monomer)	34	666
Isopropyl Amine	32	676
Monoethyl Amine	17	687
N-Pentane / 1-Pentene	36 / 30	605 / 608
Iso-Pentane	27,7	613
Neo-pentane	9,5	597
Propylene Oxide (PO)	34	817
Ethylene Oxide/Propylene Oxide mix (max 30% EO)	27	817
Vinyl Ethyl Ether	36	750
Pentenes	30,1	632,3
Dimethyl Ether	-24,8	734

1.2

1.3

1.4

Transport and Carriage Conditions

1.5 Minimum allowable tank temperature

1.6 Maximum Permissible tank pressure

1.7 List Number of grades that can be loaded/discharged simultaneously and completely segregated without risk of contamination?

List the Number of grades that can be carried simultaneously and completely segregated without risk of contamination?

What is the Number of Products that can be conditioned by reliquefaction simultaneously?

-104	Deg. Celsius
6.1	Bar gauge
2	
2	
2	
3	

B2 CARGO State the number of natural segregation's (NB: Separation must be by the removal of spools or the insertion of blanks)

2.1

2.2

2.2.1

2.2.2 Type and materials of cargo tanks

2.3 Maximum allowable relief valve setting

2.4 IMO Setting

2.5 USCG Setting

2.6 Safety valve set pressure, - if variable stipulate range of pilot valves

2.7 Maximum allowable vacuum

Maximum cargo density at 15 deg Celsius

Low alloy 5% Ni Steel (X12Ni5 or Similar)		Bar gauge
	6.1	Bar gauge
	6.1	Bar gauge
	3.9	Bar gauge
	3.9; 6.1	Kg/m3
	-0,25	Deg Cel / Hour
	972	

Maximum rate of cool-down
State any limitations regarding partially filled tanks

10

2.8

No sloshing limitations

State allowable combinations of filled and empty tanks

Any combinations of filled and empty cargo tanks are allowed but subject to check of Bending
Shearing Forces being less than the maximum permissible values which have been indicated by

B3 CARGO TANK CAPACITIES

Tank number / location

Capacity m3 (100%)
 Capacity 98%
 N-Butane capacity 98%
 N-Butane temperature
 C-Propane capacity 98%
 C-Propane temperature
 Butadiene capacity
 Butadiene temperature
 Propylene capacity
 Propylene temperature
 Vinyl Chloride Monomer capacity
 Vinyl Chloride Monomer temperature
 Ethylene capacity
 Ethylene temperature
 Propylene Oxide capacity
 Propylene Oxide temperature
 Ammonia capacity
 Ammonia temperature

CT 1	
4019,582	m3
3939,19	m3
2371,00	Tonnes
-0,5	Deg. C
2297,00	Tonnes
-45	Deg. C
2562,00	Tonnes
-4,5	Deg. C
2399,00	Tonnes
-48	Deg. C
3817,00	Tonnes
-13,8	Deg. C
2237,00	Tonnes
-103,8	Deg. C
2499,00	Tonnes
20	Deg. C
2653,00	Tonnes
-33,8	Deg. C

Tank number / location

Capacity m3 (100%)
 Capacity 98%
 N-Butane capacity 98%
 N-Butane temperature
 C-Propane capacity 98%
 C-Propane temperature
 Butadiene capacity
 Butadiene temperature
 Propylene capacity
 Propylene temperature
 Vinyl Chloride Monomer capacity
 Vinyl Chloride Monomer temperature
 Ethylene capacity
 Ethylene temperature
 Propylene Oxide capacity
 Propylene Oxide temperature
 Ammonia capacity
 Ammonia temperature

CT 2	
4020,181	m3
3939,777	m3
2371,00	Tonnes
-0,5	Deg. C
2297,00	Tonnes
-45	Deg. C
2562,00	Tonnes
-4,5	Deg. C
2400,00	Tonnes
-48	Deg. C
3818,00	Tonnes
-13,8	Deg. C
2238,00	Tonnes
-103,8	Deg. C
2499,00	Tonnes
20	Deg. C
2653,00	Tonnes
-33,8	Deg. C

Tank number / location

Capacity m3 (100%)
 Capacity 98%
 N-Butane capacity 98%
 N-Butane temperature
 C-Propane capacity 98%
 C-Propane temperature
 Butadiene capacity
 Butadiene temperature
 Propylene capacity
 Propylene temperature
 Vinyl Chloride Monomer capacity
 Vinyl Chloride Monomer temperature
 Ethylene capacity
 Ethylene temperature
 Propylene Oxide capacity
 Propylene Oxide temperature

CT 3	
4017,30	m3
3939,95	m3
2369,00	Tonnes
-0,5	Deg. C
2295,00	Tonnes
-45	Deg. C
2560,00	Tonnes
-4,5	Deg. C
2398,00	Tonnes
-48	Deg. C
3815,00	Tonnes
-13,8	Deg. C
2236,00	Tonnes
-103,8	Deg. C
2499,00	Tonnes
20	Deg. C

Ammonia capacity	2652,00	Tonnes
Ammonia temperature	-33,8	Deg. C

Tank number / location

N/A		
Capacity m3 (100%)		m3
Capacity 98%		m3
Butane capacity		Tonnes
Butane temperature		Deg. C
Propane capacity		Tonnes
Propane temperature		Deg. C
Butadiene capacity		Tonnes
Butadiene temperature		Deg. C
Propylene capacity		Tonnes
Propylene temperature		Deg. C
Vinyl Chloride Monomer capacity		Tonnes
Vinyl Chloride Monomer temperature		Deg. C
Ethylene capacity		Tonnes
Ethylene temperature		Deg. C
Propylene Oxide capacity		Tonnes
Propylene Oxide temperature		Deg. C
Ammonia capacity		Tonnes
Ammonia temperature		Deg. C

Tank number / location

N/A		
Capacity m3 (100%)		m3
Capacity 98%		m3
Butane capacity		Tonnes
Butane temperature		Deg. C
Propane capacity		Tonnes
Propane temperature		Deg. C
Butadiene capacity		Tonnes
Butadiene temperature		Deg. C
Propylene capacity		Tonnes
Propylene temperature		Deg. C
Vinyl Chloride Monomer capacity		Tonnes
Vinyl Chloride Monomer temperature		Deg. C
Ethylene capacity		Tonnes
Ethylene temperature		Deg. C
Propylene Oxide capacity		Tonnes
Propylene Oxide temperature		Deg. C
Ammonia capacity		Tonnes
Ammonia temperature		Deg. C

Tank number / location

N/A		
Capacity m3 (100%)		m3
Capacity 98%		m3
Butane capacity		Tonnes
Butane temperature		Deg. C
Propane capacity		Tonnes
Propane temperature		Deg. C
Butadiene capacity		Tonnes
Butadiene temperature		Deg. C
Propylene capacity		Tonnes
Propylene temperature		Deg. C
Vinyl Chloride Monomer capacity		Tonnes
Vinyl Chloride Monomer temperature		Deg. C
Ethylene capacity		Tonnes
Ethylene temperature		Deg. C
Propylene Oxide capacity		Tonnes
Propylene Oxide temperature		Deg. C

Ammonia capacity		Tonnes
Ammonia temperature		Deg. C

Tank number / location

Capacity m3 (100%)	N/A	m3
Capacity 98%		m3
Butane capacity		Tonnes
Butane temperature		Deg. C
Propane capacity		Tonnes
Propane temperature		Deg. C
Butadiene capacity		Tonnes
Butadiene temperature		Deg. C
Propylene capacity		Tonnes
Propylene temperature		Deg. C
Vinyl Chloride Monomer capacity		Tonnes
Vinyl Chloride Monomer temperature		Deg. C
Ethylene capacity		Tonnes
Ethylene temperature		Deg. C
Propylene Oxide capacity		Tonnes
Propylene Oxide temperature		Deg. C
Ammonia capacity		Tonnes
Ammonia temperature		Deg. C

Tank number / location

Capacity m3 (100%)	N/A	m3
Capacity 98%		m3
Butane capacity		Tonnes
Butane temperature		Deg. C
Propane capacity		Tonnes
Propane temperature		Deg. C
Butadiene capacity		Tonnes
Butadiene temperature		Deg. C
Propylene capacity		Tonnes
Propylene temperature		Deg. C
Vinyl Chloride Monomer capacity		Tonnes
Vinyl Chloride Monomer temperature		Deg. C
Ethylene capacity		Tonnes
Ethylene temperature		Deg. C
Propylene Oxide capacity		Tonnes
Propylene Oxide temperature		Deg. C
Ammonia capacity		Tonnes
Ammonia temperature		Deg. C

Total Capacity of all cargo tanks (100%)	12057,063	m3
Total Capacity of all cargo tanks (98%)	11815,921	m3
Total Capacity of N-Butane	7111,00	Tonnes
Total Capacity of C-Propane	6889,00	Tonnes
Total Capacity of Butadiene	7684,00	Tonnes
Total Capacity of Propylene	7197,00	Tonnes
Total Capacity of Vinyl Chloride Monomer	11450,00	Tonnes
Total Capacity of Ethylene	6711,00	Tonnes
Total Capacity of Propylene Oxide	7497,00	Tonnes
Total Capacity of Ammonia	7958,00	Tonnes

B16 DECK TANK CAPACITIES

Are Deck pressure tank(s) fitted?	No
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Material of tank(s)	N/A	
Maximum allowable relief valve setting	N/A	Bar gauge
Deck tank number 1 - capacity (100%)	N/A	m3
Capacity 98%		m3
Propane Capacity		Tonnes
Butane Capacity		Tonnes
Propylene capacity		Tonnes
Ethylene capacity		Tonnes
Ammonia Capacity		Tonnes
Deck tank number 2 - capacity (100%)	N/A	m3
Capacity 98%		m3
Propane Capacity		Tonnes
Butane Capacity		Tonnes
Propylene capacity		Tonnes
Ethylene capacity		Tonnes
Ammonia Capacity		Tonnes

B4 LOADING RATES

4.1

From Refrigerated Storage (Fully Refrigerated at Vessel's Manifold)

N-Butane - with vapour return	722	Tonnes/hour
N-Butane - without vapour return	722	Tonnes/hour
C-Propane - with vapour return	700	Tonnes/hour
C-Propane - without vapour return	700	Tonnes/hour
Butadiene - with vapour return	780	Tonnes/hour
Butadiene - without vapour return	780	Tonnes/hour
Propylene - with vapour return	731	Tonnes/hour
Propylene - without vapour return	731	Tonnes/hour
Ethylene - with vapour return	682	Tonnes/hour
Ethylene - without vapour return **)	682	Tonnes/hour
Ammonia - with vapour return	808	Tonnes/hour
Ammonia - without vapour return	808	Tonnes/hour
Vinyl Chloride Monomer - with vapour return	1163	Tonnes/hour
Vinyl Chloride Monomer - without vapour return	1163	Tonnes/hour
Propylene Oxide - with vapour return	1000	Tonnes/hour
Propylene Oxide - without vapour return	N/A	Tonnes/hour

4.8

From Pressure Storage

N-Butane 0 deg C - with vapour return	724	Tonnes/hour
0 deg C - without vapour return	724	Tonnes/hour
10 deg C - with vapour return	710	Tonnes/hour
10 deg C - without vapour return	710	Tonnes/hour
20 deg C - with vapour return	696	Tonnes/hour
20 deg C - without vapour return	696	Tonnes/hour
C-Propane minus 30 deg C - with vapour return	682	Tonnes/hour
Minus 30 deg C - without vapour return	682	Tonnes/hour
Minus 20 deg C - with vapour return	666	Tonnes/hour
Minus 20 deg C - without vapour return	666	Tonnes/hour
Minus 10 deg C - with vapour return	652	Tonnes/hour
Minus 10 deg C - without vapour return	652	Tonnes/hour
0 deg C - with vapour return	636	Tonnes/hour
0 deg C - without vapour return	636	Tonnes/hour
10 deg C - with vapour return by compressors	623	Tonnes/hour
10 deg C - without vapour return	276	Tonnes/hour

20 deg C - with vapour return by compressors	375	Tonnes/hour
20 deg C - without vapour return	108	Tonnes/hour
Butadiene 0 deg C - with vapour return	766	Tonnes/Hr.
0 deg C - without vapour return	766	Tonnes/Hr.
10 deg C - with vapour return	751	Tonnes/Hr.
10 deg C - without vapour return	751	Tonnes/Hr.
20 deg C - with vapour return	737	Tonnes/Hr.
20 deg C - without vapour return	737	Tonnes/Hr.
Propylene minus 30 deg C - with vapour return	703	Tonnes/Hr.
Minus 30 deg C - without vapour return	703	Tonnes/Hr.
Minus 20 deg C - with vapour return	689	Tonnes/Hr.
Minus 20 deg C - without vapour return	689	Tonnes/Hr.
Minus 10 deg C - with vapour return	672	Tonnes/Hr.
Minus 10 deg C - without vapour return	672	Tonnes/Hr.
0 deg C - with vapour return	655	Tonnes/Hr.
0 deg C - without vapour return	655	Tonnes/Hr.
10 deg C - with vapour return by compressors	638	Tonnes/Hr.
10 deg C - without vapour return	185	Tonnes/Hr.
20 deg C - with vapour return by compressors	390	Tonnes/Hr.
20 deg C - without vapour return	94	Tonnes/Hr.
Ethylene minus 100 deg C - with vapour return	684	Tonnes/Hr.
Minus 100 deg C - without vapour return **)	684	Tonnes/Hr.
Minus 95 deg C - with vapour return	674	Tonnes/Hr.
Minus 95 deg C - without vapour return **)	674	Tonnes/Hr.
Minus 90 deg C - with vapour return	666	Tonnes/Hr.
Minus 90 deg C - without vapour return **)	666	Tonnes/Hr.
Minus 85 deg C - with vapour return	658	Tonnes/Hr.
Minus 85 deg C - without vapour return **)	658	Tonnes/Hr.
Ammonia minus 30 deg C - with vapour return	725	Tonnes/Hr.
0 deg C - without vapour return	725	Tonnes/Hr.
10 deg C - with vapour return	710	Tonnes/Hr.
10 deg C - without vapour return	610	Tonnes/Hr.
20 deg C - with vapour return	690	Tonnes/Hr.
20 deg C - without vapour return	430	Tonnes/Hr.
VCM minus 10 deg C - with vapour return	1153	Tonnes/Hr.
Minus 10 deg C - without vapour return	1153	Tonnes/Hr.
0 deg C - with vapour return	1134	Tonnes/Hr.
0 deg C - without vapour return	1134	Tonnes/Hr.
10 deg C - with vapour return	1114	Tonnes/Hr.
10 deg C - without vapour return	1114	Tonnes/Hr.
20 deg C - with vapour return	1093	Tonnes/Hr.
20 deg C - without vapour return	1093	Tonnes/Hr.

4.14

Special remarks:

*) Based on +20 degC air/SW temperature
**) Tanks gassed up and cooled down
Maximum allowed P.O. cargo quantity per each tank is 3000 cub.m.

B5 DISCHARGING - GENERAL

5.1	Cargo Pumps	
5.2	Type of Pumps	Hamworthy Svanehoj DW 200/200-3-K+I
5.3	Number of pumps per tank	1
5.4	Rate per Pump	400 m3/hr

5.5	At Delivery Head mlc	120	mlc
	Maximum density	972	Kg/m3

5.6 Booster Pump

5.7	Type of Booster Pumps	Hamworthy Svanehoj NMB 150c	
5.8	Number of pumps	2	
5.9	Rate per Pump	400	m3/hr
5.10	At Delivery Head mlc	120	mlc
	Maximum density	650	kg/m3

Copies of pumping curves for cargo and booster pumps are enclosed?

YES

B6 DISCHARGE PERFORMANCE

Full Cargo Discharge Times per tank (using 2 cargo pumps and 1 booster pump)	10	Hours
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Fully Refrigerated

Manifold Back Press 1 kP/cm2, with vapour return	10	Hours
Manifold Back Press 1 kP/cm2, without vapour return	10	Hours
Manifold Back Press 5 bar g - Ammonia - DW pump	10	Hours
Manifold Back Press 5 bar g - C-Propane - DW pump	10	Hours
Manifold Back Press 10 kP/cm2, with vapour return	10	Hours
Manifold Back Press 10 kP/cm2, without vapour return	10	Hours

Pressurised

Manifold Back Press 1 kP/cm2, with vapour return	10	Hours
Manifold Back Press 1 kP/cm2, without vapour return	10	Hours
Manifold Back Press 5 bar g - Ammonia 0.9 bar g - DW pump	10	Hours
Manifold Back Press 5 kg/cm2, without vapour return	10	Hours
Manifold Back Press 10 bar g - C-Propane 4.8 bar g - DW pump	10	Hours
Manifold Back Press 10 bar g - Ammonia 0.9 bar g - DW pump	50	Hours

B7 UNPUMPABLES

7.1	Tank number / location	1	1	m3
	Tank number / location	2	1	m3
	Tank number / location	3	1	m3
	Tank number / location			m3
	Tank number / location			m3
	Tank number / location			m3
	Tank number / location			m3
	Tank number / location			m3
	Total		3	m3

B8 VAPORISING UNPUMPABLES

8.1	Process used	Hot Gas	
8.2	Time to vaporise liquid unpumpables remaining after full cargo discharge of (1 CT, 1 Compressor running):		
8.3	Butane	2,5	Hours
8.4	Propane	1,5	Hours
8.5	Butadiene	3	Hours
8.6	Propylene	1,5	Hours
8.7	Ethylene	1,5	Hours
8.8	Ammonia	6	Hours
8.9	Vinyl Chloride Monomer	3	Hours
	Propylene Oxide	N/A	Hours

B9 RELIQUEFACTION PLANT

9.1

9.3	Plant Design Conditions - air temperature	45	Deg. C
	Plant Design Conditions - sea temperature	32	Deg. C
9.4	Plant Type		
9.5	Is the plant single stage/direct? (for warm cargoes):	YES	
9.6	Is the plant two stage/direct? (for propane, propylene and ammonia):	YES	
9.7	Is the plant simple cascade?	YES	
	Coolant type	R-404A	
9.8	Compressors		
9.8.1	Compressor type	Receiprocating / labyrinth	
9.9	Compressor makers name	Burckhardt Compression 2K 140-2A	
9.10	Number of compressors	3	
9.11	Capacity per unit, 1st / 2nd stage (swept volume)	1260 / 510	m3/hr
	Are they Oil Free?	YES	

B11 CARGO TEMPERATURE LOWERING CAPABILITY (AT SEA WITH SEA TEMPERATURE +15C)

11.1	Time taken to lower the temperature of:		
11.2	C-Propane from -5 deg C to - 42 deg C	161	Hours
11.3	C-Propane from -20 deg C to - 42 deg C	117	Hours
11.4	C-Propane from -38 deg C to - 42deg C	35	Hours
11.5	C-Propane from +20 deg C to -0.50 deg C	N/A	Hours
	C-Propane from 0 deg C to -20 deg C	66	Hours
11.6			
11.7	N-Butane from +20 deg C to-0.5 deg C	85	Hours
11.8	N-Butane from +10 deg C to-0.5 deg C	67	Hours
	N-Butane from +10 deg C to -5 deg C	N/A	Hours
11.9			
	Butadiene		
	From +20 deg C to -5 deg C	98	Hours
11.10			
	Propylene		
	From -20 deg C to -47 deg C	130	Hours
11.11			
	Ethylene		
	From -99 deg C to -103 deg C	58	Hours
11.12			
	Ammonia		
	From -16 deg C to -33 deg C	181	Hours
11.13			
	Vinyl Chloride Monomer		
	From -5 deg C to -14 deg C	72	Hours

B12 INERT GAS AND NITROGEN

12.1	Main IG Plant		
12.2	Type of system	N/A	
12.3	Capacity		
12.4	Type of fuel used		
	Composition of IG - oxygen		
	Composition of IG - CO2		
	Composition of IG - Nox		
12.5	Composition of IG - N2		
12.6	Lowest dewpoint achievable		
	Used for		
12.7	Nitrogen plant		
12.8	Type of System	Nitrogen generator, Gazcon 3xMN1000	
12.9	Purity N2	95%	
	Capacity	1450 M3/Hr	

	Purity N2	99,50%	
	Capacity	1000 M3/Hr	
12.10	Purity N2	99,90%	
12.11	Capacity	700 M3/Hr	
	Used for	Inerting and Gas freeing	
12.12	Nitrogen		
12.13	Liquid storage capacity	720	LTR
12.14	Daily boil-off loss	nil	
12.15	Maximum supply pressure	0,3	Bar
12.16	Supply capacity		
	Used for	Nitrogen padding	

B13 CARGO TANK INERTING/DE-INERTING

13.1			
13.2	Time taken to inert from fresh air to under 5% O2 at minus 25 degree C?	17	Hours
	Time taken to inert from cargo vapour to fully inert at minus 25 degrees dewpoint when IG density is less than product?	40	Hours
	Time taken to inert from cargo vapour to fully inert at minus 25 degrees dewpoint when IG density is greater than product?	40	Hours

B14 GAS FREEING TO FRESH AIR

14.1			
14.2	Plant used	Nitrogen Plant	
	Time taken from fully inert condition to fully breathable fresh air?	14	Hours

B15 CHANGING CARGO GRADES

Indicate number of hours needed to change grades from the removal of pumpables to tanks fit to load and the estimated quantity of Inert Gas and or Nitrogen consumed during the operation:

	Hours	Air	Nitrogen
From C-Propane to N-Butane	77	37 000 Nm3	46 000 Nm3
From C-Propane to Butadiene	77	37 000 Nm3	46 000 Nm3
From C-Propane to Ethylene	90	37 000 Nm3	46 000 Nm3
From C-Propane to Ammonia	77	37 000 Nm3	46 000 Nm3
From C-Propane to Vinyl Chloride Monomer	77	37 000 Nm3	46 000 Nm3
From C-Propane to Propylene Oxide	60	37 000 Nm3	46 000 Nm3
From N-Butane to C-Propane	77	37 000 Nm3	46 000 Nm3
From N-Butane to Butadiene	77	37 000 Nm3	46 000 Nm3
From N-Butane to Ethylene	90	37 000 Nm3	46 000 Nm3
From N-Butane to Ammonia	77	37 000 Nm3	46 000 Nm3
From N-Butane to Vinyl Chloride Monomer	77	37 000 Nm3	46 000 Nm3
From N-Butane to Propylene Oxide	60	37 000 Nm3	46 000 Nm3
From Butadiene to C-Propane	77	37 000 Nm3	46 000 Nm3
From Butadiene to N-Butane	77	37 000 Nm3	46 000 Nm3
From Butadiene to Ethylene	90	37 000 Nm3	46 000 Nm3
From Butadiene to Ammonia	77	37 000 Nm3	46 000 Nm3
From Butadiene to Vinyl Chloride Monomer	77	37 000 Nm3	46 000 Nm3
From Butadiene to Propylene Oxide	60	37 000 Nm3	46 000 Nm3
From Ethylene to C-Propane	90	37 000 Nm3	46 000 Nm3
From Ethylene to N-Butane	90	37 000 Nm3	46 000 Nm3
From Ethylene to Butadiene	140	37 000 Nm3	46 000 Nm3
From Ethylene to Ammonia	60	37 000 Nm3	46 000 Nm3
From Ethylene to Vinyl Chloride Monomer	90	37 000 Nm3	46 000 Nm3
From Ethylene to Propylene Oxide	60	37 000 Nm3	46 000 Nm3
From Ammonia to C-Propane	77	37 000 Nm3	46 000 Nm3
From Ammonia to N-Butane	77	37 000 Nm3	46 000 Nm3
From Ammonia to Butadiene	77	37 000 Nm3	46 000 Nm3

From Ammonia to Ethylene
 From Ammonia to Vinyl Chloride Monomer
 From Ammonia to Propylene Oxide
 From Vinyl Chloride Monomer to C-Propane
 From Vinyl Chloride Monomer to N-Butane
 From Vinyl Chloride Monomer to Butadiene
 From Vinyl Chloride Monomer to Ammonia
 From Vinyl Chloride Monomer to Ethylene
 From Vinyl Chloride Monomer to Propylene Oxide
 From Propylene Oxide to C-Propane
 From Propylene Oxide to N-Butane
 From Propylene Oxide to Butadiene
 From Propylene Oxide to Ethylene
 From Propylene Oxide to Vinyl Chloride Monomer
 From Propylene Oxide to Ammonia

90	37 000 Nm3	46 000 Nm3
77	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
77	37 000 Nm3	46 000 Nm3
77	37 000 Nm3	46 000 Nm3
77	37 000 Nm3	46 000 Nm3
77	37 000 Nm3	46 000 Nm3
90	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3
60	37 000 Nm3	46 000 Nm3

Cargo Grade Change Operations that cannot be carried out at sea:

All operation can be carried out at sea but have to load small parcel for gassing up/ coolong down purpose.

B17 PRE-LOADING COOLDOWN

17.1	The following questions ask the Time and Quantity of coolant required to cooldown cargo tanks from Propane - Quantity of Coolant Required Propane - Time required to cooldown cargo tanks from ambient temperature with vapour return line Propane - Time required to cooldown cargo tanks from ambient temperature without vapour return line	70 cub.m. 40 56	
17.2	Butane - Quantity of Coolant Required Butane - Time required to cooldown cargo tanks from ambient temperature with vapour return line Butane - Time required to cooldown cargo tanks from ambient temperature without vapour return line	50 cub.m. 28 32	
17.3	Butadiene - Quantity of Coolant Required Butadiene - Time required to cooldown cargo tanks from ambient temperature with vapour return line Butadiene - Time required to cooldown cargo tanks from ambient temperature without vapour return line	60 cub.m. 36 40	
17.4	Propylene - Quantity of Coolant Required Propylene - Time required to cooldown cargo tanks from ambient temperature without vapour return line Propylene - Time required to cooldown cargo tanks from ambient temperature with vapour return line	75 cub.m. 36 40	
17.5	Ethylene - Quantity of Coolant Required Ethylene - Time required to cooldown cargo tanks from ambient temperature with vapour return line Ethylene - Time required to cooldown cargo tanks from ambient temperature without vapour return line	80 cub.m. 72 84	Tons Hours
17.6	Ammonia - Quantity of Coolant Required	75 cub.m.	

17.7	Ammonia - Time required to cooldown cargo tanks from ambient temperature with vapour return line	36	
	Ammonia - Time required to cooldown cargo tanks from ambient temperature without vapour return line	40	
	VCM - Quantity of Coolant Required	70 cub.m.	
	VCM - Time required to cooldown cargo tanks from ambient temperature without vapour return line	60	
	VCM - Time required to cooldown cargo tanks from ambient temperature with vapour return line	72	

B18 LPG VAPORISER

18.1			
18.2	Type of Vaporiser	U-tubes, welded in tube plate	
18.3	Number of Vaporisers fitted	1	
18.4	Capacity per unit - C-Propane	2500	Nm3/h
18.5	Liquid Supply Rate	8	m3/h
18.6	Delivery Temperature	-42	degC
18.7	Capacity per unit - Ammonia	2500	Nm3/h
18.8	Liquid Supply Rate	3	m3/h
18.9	Delivery Temperature	-33	degC
18.10	Capacity per unit - Nitrogen	NA	Nm3/h
18.11	Liquid Supply Rate	NA	m3/h
	Delivery Temperature	NA	degC

B19 BLOWER

19.1		
19.2	Type of Blower	
19.3	Rated Capacity	
	Delivery Pressure	

B20 CARGO RE-HEATER

20.1			
20.2	Type of Re-Heater	U-tubes, welded in tube plate	
20.3	Number Fitted	1	
20.4	Heating Medium	Seawater	
20.5	Discharge rates with seawater at 15 degC to raise product temperature of Propane from -42 degC to 0 degC	500	m3/h
	Discharge rates with seawater at 15 deC to raise product temperature of Ammonia from -33 degC to 0 degC	280	m3/h

B21 HYDRATE CONTROL

21.1			
21.1.1	Type of Depressant?	Ethanol	
21.2	Freezing point temperature?	-114	
21.3	Quantity of Depressant Carried?	200	Ltr.
	Means of injection?	Portable pump	
	Name any other system used	Hot gas	

B22 CARGO MEASUREMENT

22.1	Level Gauges	
22.2	Are level gauges local or remote?	Both
22.3	Name of manufacture	Henri Systems Holland B.V.
22.4	Type	FTLG 807 SUS
22.5	Rated Accuracy	+/- 3 mm
	Certifying Authority	N/A
22.6	Temperature Gauges	
22.7	Name of manufacture	Teck Skoteslv
22.8	Type	Type TXC

22.9	Rated Accuracy	±1% x F.S.
	Certifying Authority	N/A
22.10	Pressure Gauges	
22.11	Name of manufacture	Teck Skoteslv
22.12	Type	Type IM
22.13	Rated Accuracy	±1% x F.S.
	Certifying Authority	N/A
22.14	Oxygen Analyser	
22.15	Name of manufacture	Riken Keiki
22.15.1	Type	GX-8000E
	What is the lowest level measurable?	0%
22.16	Fixed Gas Analyser	
22.17	Name of manufacture	Omicron
	Type	OGS 3.11
22.18	Cargo Tank Calibrations	
22.19	Are Cargo tank calibration tables available?	Yes
22.20	Name of Measuring Company	SGS South Korea
22.21	Name of Certifying Authority	
22.21.1	Calibration calculated to cm?	NO
22.22	Calibration calculated to 1/2 cm?	YES
22.22.1	Tables established to cm?	NO
22.22.2	Tables established to mm?	YES
22.23	Tables established to "other" (state what other)	N/A
22.24	Are trim and list corrections available?	YES
22.25	Are temperature corrections available?	YES
	Are float gauge tape corrections available?	YES

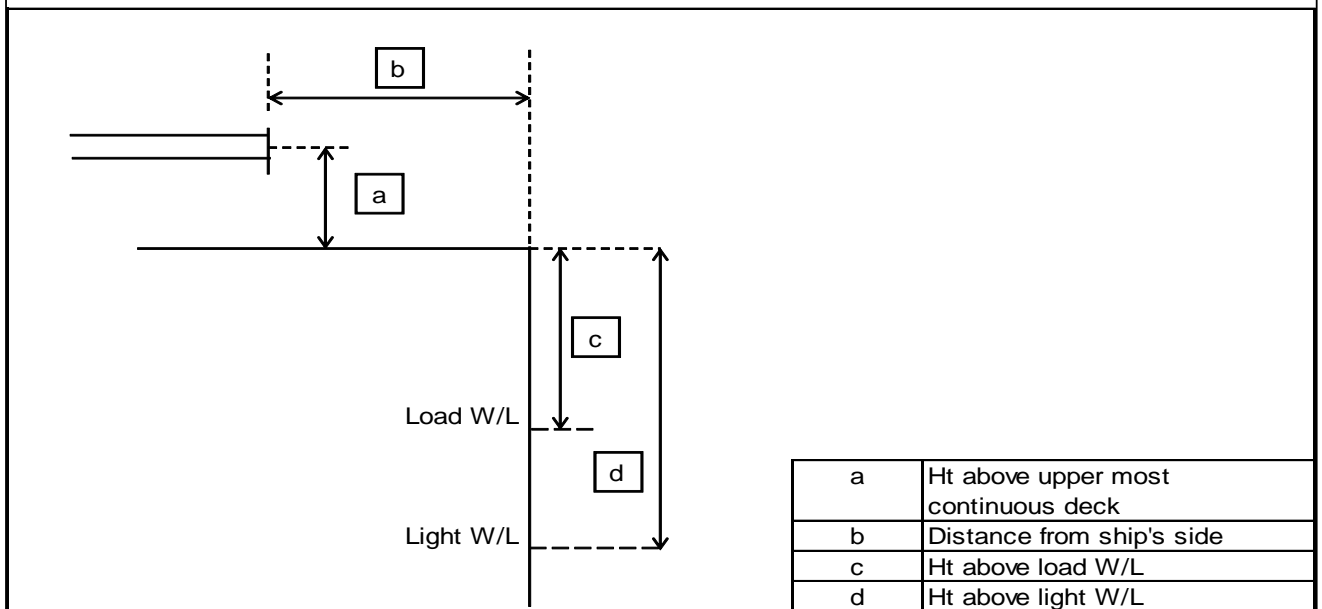
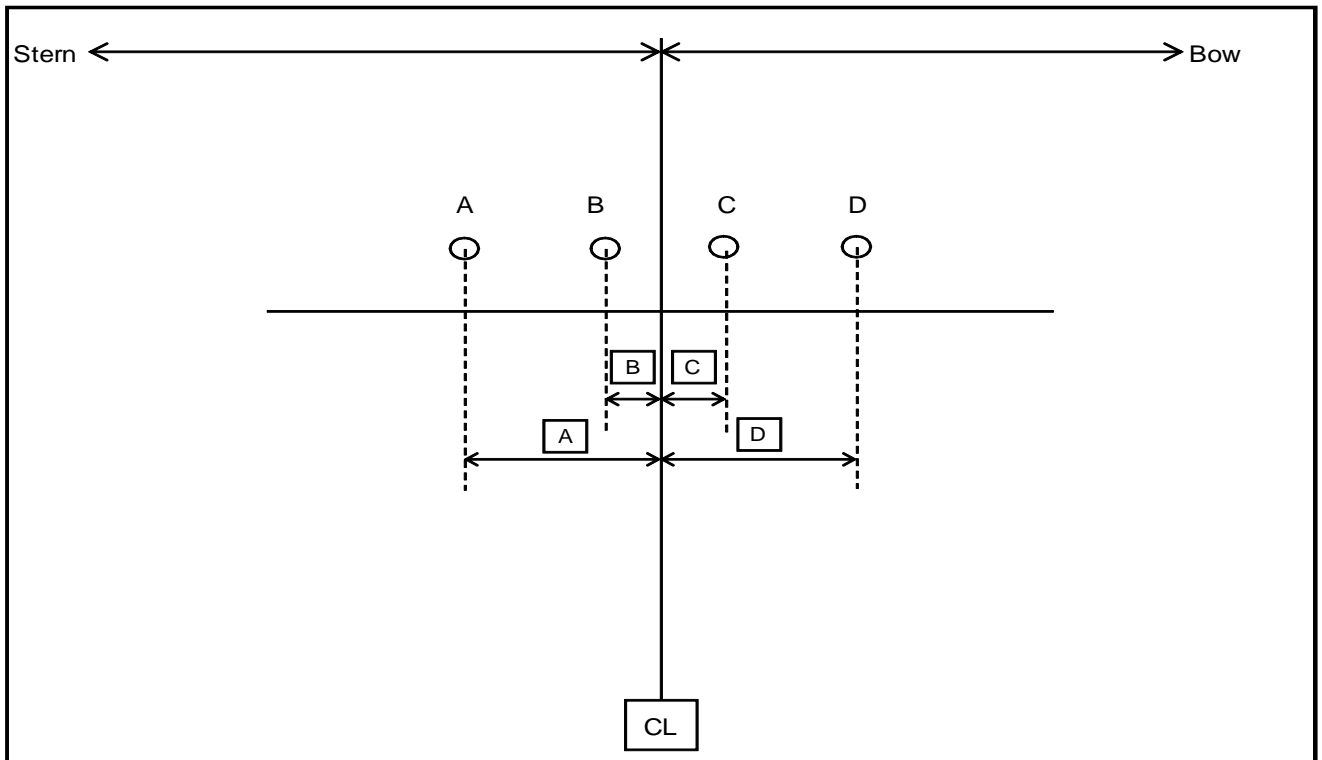
B23 CARGO SAMPLING

23.1	May cargo samples be obtained from the levels; top, middle and bottom in all cargo tanks?	Yes
	If no, - the arrangement for sampling is limited to:	
23.2	Can samples be drawn from tank vapour outlet?	NO
	Can samples be drawn from manifold liquid line?	NO
	Can samples be drawn from manifold vapour line?	NO
23.3	Can samples be drawn from pump discharge line?	YES
	State sample connection type	NPT 1/2" FEMALE CONNECTOR

Size of sample connection

1/2"

B24 CARGO MANIFOLD



Center of manifold to bow
Center of manifold to stern

74,00	M
68,54	M

Liquid line L1 (D)

Distance from bow
Distance from stern
Distance from manifold centerline (D)
Size and rating

71,70	M
70,84	M
2,30	M
8" / ANSI 300	

Type	Flat	
Height above uppermost continuous deck	2,75	M
Distance from ship's side	2,55	M
Height above load waterline	5,36	M
Height above light waterline	11,13	M
Vapour line V1 (C)		
Distance from bow	73,15	M
Distance from stern	69,39	M
Distance from manifold centerline (C)	0,85	M
Size and rating	6" / ANSI 300	
Type	Flat	
Height above uppermost continuous deck	2,75	M
Distance from ship's side	2,55	M
Height above load waterline	5,36	M
Height above light waterline	11,13	M
Vapour line V2 (B)		
Distance from bow	74,85	M
Distance from stern	67,69	M
Distance from manifold centerline (B)	0,85	M
Size and rating	6" / ANSI 300	
Type	Flat	
Height above uppermost continuous deck	2,75	M
Distance from ship's side	2,55	M
Height above load waterline	5,36	M
Height above light waterline	11,13	M
Liquid line L2 (A)		
Distance from bow	76,35	M
Distance from stern	66,19	M
Distance from manifold centerline (A)	2,35	M
Size and rating	10" / ANSI 300	
Type	Flat	
Height above uppermost continuous deck	2,75	M
Distance from ship's side	2,55	M
Height above load waterline	5,36	M
Height above light waterline	11,13	M
Liquid line L3		
Distance from bow	N/A	
Distance from stern		
Distance from manifold centerline		
Size and rating		
Type		
Height above uppermost continuous deck		
Distance from ship's side		
Height above load waterline		
Height above light waterline		
Vapour line V3		
Distance from bow	N/A	
Distance from stern		
Distance from manifold centerline		
Size and rating		
Type		
Height above uppermost continuous deck		
Distance from ship's side		
Height above load waterline		
Height above light waterline		
Vapour line V4		
Distance from bow	N/A	
Distance from stern		
Distance from manifold centerline		
Size and rating		
Type		
Height above uppermost continuous deck		

Distance from ship's side	
Height above load waterline	
Height above light waterline	
Liquid line L4	
Distance from bow	N/A
Distance from stern	
Distance from manifold centerline	
Size and rating	
Type	
Height above uppermost continuous deck	
Distance from ship's side	
Height above load waterline	
Height above light waterline	
Nitrogen manifold	
Distance from bow	N/A
Distance from stern	
Distance from manifold centerline	
Size	
Height above uppermost continuous deck	
Distance from ship's side	

Manifold Arrangement Located on Top of Compressor

Distance from rail of compressor room/platform to presentation flanges	N/A
Distance from deck of compressor room/platform/try to centre of manifold	N/A

B25 CARGO MANIFOLD REDUCERS

25.1	Number of ANSI Class 300 reducers carried onboard	15	
	Flange rating of ANSI Class 300 reducer	ANSI B16.5 WN RF	
	Size of ANSI Class 300 reducer	10" down to 3"	
25.2	Length of ANSI Class 300 reducer	500	MM
	Number of ANSI Class 300 to Class 150 reducers carried onboard	15	
	Flange rating of ANSI Class 300 to Class 150 reducer	ANSI B16.5 WN RF	
	Size of ANSI Class 300 to Class 150 reducer	10" down to 3"	
25.3	Length of ANSI Class 300 to Class 150 reducer	500	MM
	Number of ANSI Class 150 reducers carried onboard	N/A	
	Flange rating of Class 150 reducer		
	Size of ANSI Class 150 reducer		

Length of ANSI Class 150 reducer

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B26 CONNECTIONS TO SHORE FOR ESD AND COMMUNICATIONS SYSTEMS

26.1	Is ESD connection to shore available?	Yes	
	If yes, is the system pneumatic?	-	
	If yes, is the system electrical?	Yes	
26.2	If yes, is the system fiber optic?	-	
26.3	What is the type of connection used?	For MTL SIG04 cable	
	Are ESD hoses or cables available on board?	Pendant	
	If yes, length of pneumatic	-	
	If yes, length of electrical	30,00	M
26.4	If yes, length of fiber optic	-	
26.5	Is there a connection available for a telephone line?	No	
	Are ESD connections available on both sides of vessel?	Yes	
	Are ESD Fusible plugs fitted at tank domes?	Yes	
	Are ESD Fusible plugs fitted at manifolds?	Yes	
	Is the link compatible with the SIGTTO guidelines?	Yes	
	Type of manifold valve	Westad	Butterfly
	Closing time in seconds	Within 30 s	
	Is closing time adjustable?	Yes	
	Is Independent high level shut down system fitted(overflow control)?	Yes	
	If yes, does the independent high level shutdown system also switch off running cargo pumps?	Yes	
	Shut down level %	99	

B27 MANIFOLD DERRICK/CRANE

27.1			
27.2	Is manifold derrick provided	N/A	
27.3	Is manifold crane provided	YES	
	Is lifting equipment same for port and starboard?	YES	
27.4	If no, then stipulate details	Midship Crane	
27.4.1	State SWL at maximum outreach	5	MT
	Maximum outreach of lifting equipment	16,00	MT

B28 STORES DERRICK/CRANE

28.1	State location	Aft, midships	
	SWL	2	MT

B29 SISTER VESSEL(S)

29.1	Name of vessel	JS Greensky
		JS Greensun
		JS Greensea
		JS Greensail
		JS Greenstone
		JS Greenspeed